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Effects of surfactant on morphology, chemical properties and catalytic activity of hydroxyapatite

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Abstract

Hydroxyapatite (HAP) was synthesised in the presence of surfactants and tested as a catalyst in CO oxidation. XRD confirmed that the characteristic HAP crystal phase was practically unaffected by the addition of surfactant. The surfactant altered both the Ca/P ratio and particle size of HAP. Catalyst tests showed that the activity of HAP increased for preparations using TWEEN, PEG and PVA. The temperature for 50% conversion, T_{50} , values decreased from 340 °C for unmodified HAP, to 320 °C for TWEEN and to 315 °C for both PEG and PVA. This enhanced activity is rationalised by the higher BET surface areas and acid site densities in the surfactant-modified preparations: these increased from 52 m² g⁻¹ for HAP to 69, 76 and 68 m² g⁻¹, and from 101 μmoles g⁻¹ for HAP to 110, 170 and 126 μmoles g⁻¹ for TWEEN, PEG and PVA, respectively. These findings demonstrate that HAP i.e. without the addition of precious metals to either the surface or framework, is an active CO catalyst and that the straightforward inclusion of surfactant during preparation can optimise the catalytic performance.

Keywords: CO oxidation, hydroxyapatite, surfactant, acid strength

1. Introduction

Hydroxyapatite (HAP), $\text{Ca}_5(\text{PO}_4)_3(\text{OH})$, is a naturally occurring mineral form of calcium phosphate with interesting properties such as flexible structure, ion-exchange capacity, and the presence of both acidic and basic surface sites. It has, therefore, been of considerable interest in areas such as biomaterials [1], adsorbents [2] and catalysis [3]. HAP has been used as a precious/transition metal catalyst support in a variety of reactions including: oxidation of alcohols [4], methane [5] and CO [6]; selective reduction of NO_x over copper [7] and silver [8] impregnated HAP; Claisen-Schmidt condensation [9]; Michael addition [10]; Heck [11]; Knoevenagel condensation [12]; and the Diels-Alder reaction [13].

HAP can be synthesised using a dry process e.g. solid-state reaction [14, 15], or wet processes e.g. hydrothermal [16], precipitation [17], sol-gel [18], microemulsion [19] or reverse microemulsion [20]. However, the synthesis of high surface area HAP has been a challenge. The main problem is the agglomeration of particles, which in turn leads to HAP with irregular shapes and BET surface area

predominantly in the range 20-60 m² g⁻¹. It has been shown that BET surface areas may be increased by optimising the wet process parameters [21]. The microemulsion technique was used to produce HAP with regular shape [22]; this method employs a water/oil system mixed with at least two surfactants (Span 20 and TWEEN 80), which have a strong influence on the morphology and surface area of HAP.

To the best of our knowledge, there are no reports in the literature that correlate the morphology of HAP to its chemical properties and catalytic activity. HAP based materials have been used as supports for catalysts/metals in CO oxidation reactions. These reports usually add precious metals e.g. Au, Pt, Pd to HAP; the resulting investigation and discussion of the catalytic activity tend to focus on the precious metals rather than the underlying HAP support. Our study shows that HAP is active in CO oxidation without the addition of precious metal, either substituted into the HAP framework or dispersed as nanoparticles on the surface. Furthermore, we demonstrate that this catalytic activity can be optimised by altering the HAP surface acidity using straightforward surfactant addition during preparation.

2. Experimental

2.1 Materials

The starting materials for catalyst preparation were; calcium nitrate tetrahydrate (>99%) and ammonium hydrogen phosphate (ACS, >98%), Alfa Aesar; poly vinyl alcohol (MW 85,000-124,000, 99% hydrolysed), hexadecyltrimethylammonium-bromide (CTAB) (>99%), and TWEEN[®] 60, Sigma Aldrich; poly-ethylene-glycol 400 and polyacrylamide, Fluka and hexadecylamine (synthesis grade), Merck. Materials were used as received without further purification.

2.2 Catalyst preparation

HAP was synthesised by dissolving 23.6 g of Ca(NO₃)₂·4H₂O in 100 cm³ distilled water in a beaker to make a 1 M solution. In another beaker, 7.92 g of (NH₄)₂HPO₄ was dissolved in 100 cm³ distilled water to make a 0.6 M solution. These quantities give a Ca/P molar ratio of 1.67, which corresponds to the stoichiometry of HAP. The Ca(NO₃)₂·4H₂O solution was added dropwise to the stirred (NH₄)₂HPO₄ solution, during which pH 10 was maintained by the addition of 30 wt% NH₄OH. A white precipitate was formed, stirred for 24 h at room temperature, extracted by filtration, washed and dried at room temperature for 24 h, followed by calcination in air at 550 °C for 4 h at 5 °C min⁻¹ ramp rate. For HAP synthesised using surfactants, (NH₄)₂HPO₄ solution (same quantity and concentration as above) was added dropwise to a 2 wt% solution of surfactant prepared by dissolving the appropriate amount of surfactant reagent in 50 cm³ water followed by stirring for 1 h. The remainder of the procedure was identical to that for synthesis prepared in the absence of surfactant. Table 1 summarises the samples prepared.

2.3 Characterisation

X-ray diffraction (XRD) was conducted in powder spinning mode at ambient conditions using a Panalytical X'Pert Powder diffractometer with Cu K α radiation ($\lambda = 1.5406 \text{ \AA}$). All powder diffraction patterns were recorded over an angular range of 20 to 70° with a step size 0.052 and step time 200 s, using an X-ray tube operated at 40 kV and 30 mA with fixed 0.5 ° anti-scatter slit. Mean crystallite particle size was determined from the Scherrer equation using the (002), (211), (310), (222) and (213) crystal planes. Scanning electron microscopy (SEM) images were recorded using a ZEISS Supra 40VP microscope. Prior to imaging, the samples were sputter coated with a thin layer of gold. SEM images were taken using an acceleration voltage of 2 kV and a working distance of approximately 6 mm. Semi-quantitative chemical analysis was performed by energy-dispersive X-ray spectroscopy (EDAX) on an Apollo 40 SDD instrument using an acceleration voltage of 20 kV and a working distance of approximately 15 mm. Three areas of each sample were used. Nitrogen adsorption/desorption measurements were carried out using a Micromeritics ASAP 2020 Surface Analyser at -196 °C. Samples were degassed under vacuum ($p < 10^{-5}$ mbar) for 3 h at 300 °C prior to analysis. BET surface areas were calculated in the relative pressure range 0.05-0.30. The NH₃-TPD experiments were performed using a Quantachrome ChemBET Pulsar TPR/TPD instrument. For each measurement, approximately 50 mg of fresh sample was used and initially pretreated in 50 cm³ min⁻¹ Ar flow for 1 h at 200 °C. The catalyst was then cooled down to 30 °C where 5% NH₃/Ar with the same flow rate was introduced for 2 h. Following NH₃ adsorption, the catalyst was purged by Ar flow for 60 min to remove any gas phase and weakly bound NH₃. Finally, the temperature was increased at a rate of 5 °C min⁻¹ up to 600 °C under Ar flow at the total rate of 50 cm³ min⁻¹. The desorption of NH₃ was monitored by TCD detector. Particle size analysis was performed on a Zetasizer Nano particle size analyser using dynamic light scattering (DLS). Samples were prepared and analysed according to the method explained in literature for dispersion of nanoparticles in aqueous media [23].

Table 1. List of surfactants used for HAP synthesis

Sample number	Surfactant	Surfactant description	Surfactant type
1	No surfactant	---	---
2	PEG	Polyethylene glycol	Non-ionic
3	P213	Poly(ethylene glycol)-block-poly(propylene glycol)-block-poly(ethylene glycol)	Non-ionic
4	PVA	Polyvinyl alcohol	Non-ionic
5	TWEEN 80	Polyoxyethylene Sorbitan Monolaurate	Non-ionic
6	CTAB	Hexadecyl-trimethyl-ammonium bromide	Cationic
7	HDA	Hexadecylamine	Cationic
8	PAM	Polyacrylamide	Cationic

2.4 Catalytic tests

Catalytic activity was determined by oxidation of CO. Figure 1 illustrates the PFD of the experimental rig. Powder samples were pelletised in a die using a 5 ton hand press, crushed and sieved to particle size

<100 μm . 0.5 g of catalyst was placed in a quartz fixed-bed reactor (10 mm internal diameter, 400 mm length) and secured in the centre of the tube using quartz wool. A temperature-controlled furnace (Carbolite type 3216, Tempatron, PID500/110/330) was used to heat the reactor to the desired temperature. A feed mixture comprising $\text{CO}:\text{O}_2:\text{He}$ equal to 1:2:2 and total flow rate of $50\text{ cm}^3\text{ min}^{-1}$ was used in all catalytic tests, giving a GHSV= 1900 h^{-1} . The flow of each gas was maintained using Bronkhorst UK model F-201CV mass flow controllers. The reaction products were monitored by a Hewlett Packard 5890 series II gas chromatograph equipped with a GS-GASPRO column (60 m x 0.32 mm) connected via a 6-way gas sampling valve to a thermal conductivity detector. Measurements were recorded at $10\text{ }^\circ\text{C}$ intervals (after holding at that temperature for 5 mins) between 200 and $460\text{ }^\circ\text{C}$ using a heating rate of $10\text{ }^\circ\text{C min}^{-1}$. Samples were purged with $20\text{ cm}^3\text{ min}^{-1}$ He for 1 h at $250\text{ }^\circ\text{C}$ prior to reaction to remove any adsorbed HC, CO or moisture.

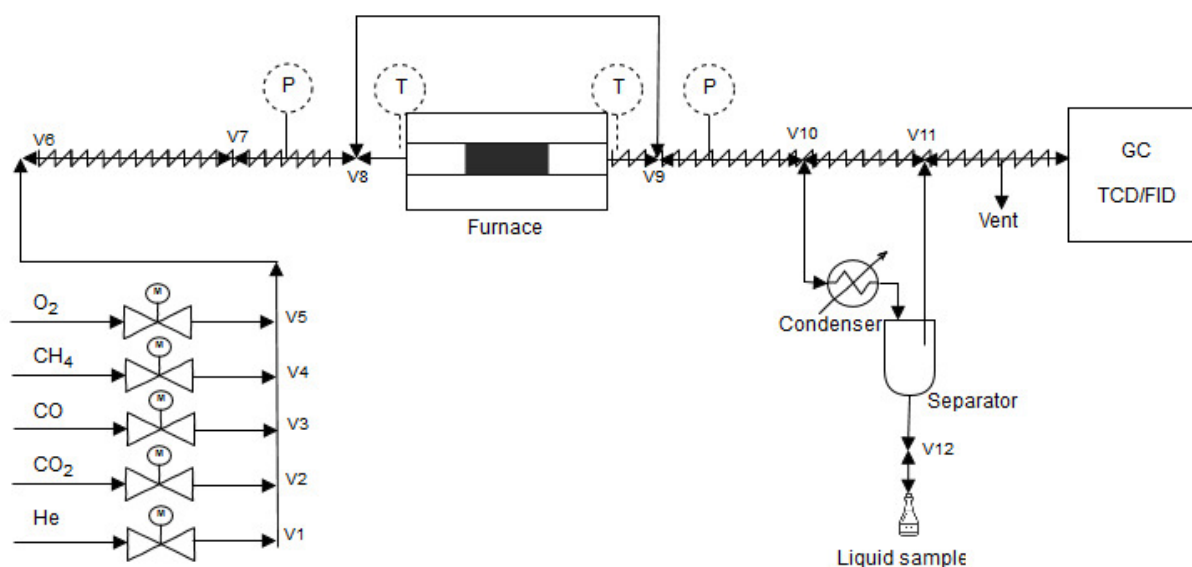


Figure 1. PFD of catalyst testing rig.

3. Results and Discussion

3.1 Characterisation

The XRD patterns, Figure 2, show that all samples exhibit the characteristic diffraction patterns consistent with the JCPDS diffraction pattern number 01-072-1243 of HAP; the XRD results also match with the NIST data for HAP prepared by Markovic et al. [24]. The diffraction lines (2θ), d -values ($d_{2\theta}$ calculated from 2θ values using the Bragg equation), relative intensities (I_{relative}), and hkl indices are listed in Table 2. Interestingly, in most cases the addition of surfactant led to a reduction in mean crystallite size, particularly so in the case of the sample prepared using P123, which was 16 nm. Although surfactants can significantly affect the size of HAP crystals, it is possible to optimise the crystallite size by altering the synthesis method. For instance, Bouyer et. al [25] investigated the effects

of temperature, pH and reactant addition rate on the morphology, surface area, purity and mean crystallite dimension of HAP. Their results suggest that, in order to obtain HAP with high purity and monocrystalline structure, reactants should be added at a ‘moderate’ rate, at temperature lower than 60 °C with a final pH above 10. They obtained HAP with crystal size of 24 nm under optimum conditions ($T = 40\text{ }^{\circ}\text{C}$, acid addition rate = $30\text{ cm}^3\text{ min}^{-1}$, $\text{pH} > 10$).

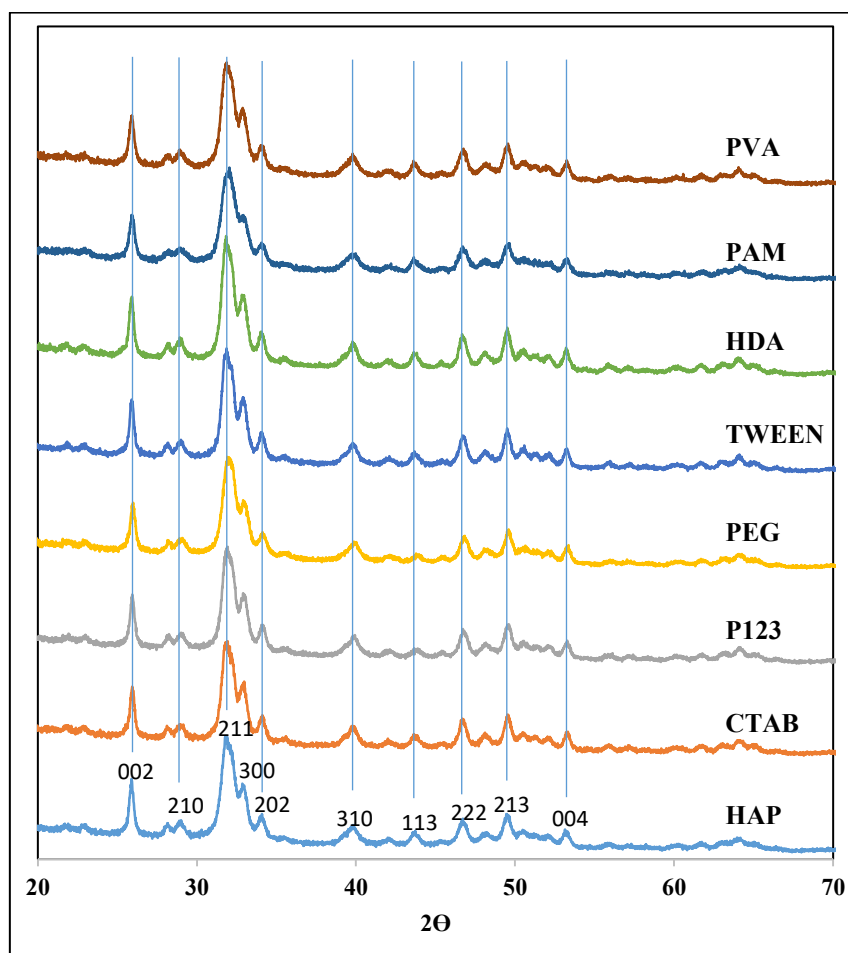


Figure 2. XRD patterns of HAP samples.

The semi-quantitative EDAX results of the different HAP samples prepared in this study, Table 3, confirm that the addition of surfactant increases the Ca/P ratio in most of the samples, from 1.66 to as high as 2.1 for PAM, while the only ratio to decrease was CTAB to 1.60. It is not possible to state with confidence whether the ratio for the PEG sample has increased slightly or remained constant, as the difference may be due to experimental error, but this does not affect the general trend towards an increased Ca/P ratio following the addition of surfactant. The Ca/P ratio plays an important role in determining chemical properties such as acid/base reactivity and ion exchange ability/capacity of the final product. In other words, it is possible to tune the properties of HAP with respect to its application by the straightforward addition of a suitable surfactant during preparation. It should be noted that the mechanical strength of HAP is related to the Ca/P ratio, reaching a maximum value at stoichiometric ratio 1.67; the mechanical strength decreases as the ratio diverges from 1.67, whereby the loss in

mechanical strength increases with the Ca/P ratio difference from 1.67 [26]. Uota et al. observed similar results in their study to prepare high surface area HAP [27]. They obtained HAP with Ca/P ratio of 2.2 using TWEEN and nonaoxyethylene dodecyl ether as surfactant. It is well known that the crystal growth of nanomaterials can be controlled by surfactant structure e.g. monomeric, micellar, vesicular, wormlike, and microemulsion, to achieve a desired structure and morphology. Surfactants are adsorbed on the crystal planes of particles and modify the interfacial energy, leading to changes in the rate and direction of crystal growth [28, 29].

Table 2. XRD data for HAP samples; $d_{2\theta}$: corresponding d-value, hkl: Miller indices, I_{relative} : relative intensity.

2θ (°)	$d_{2\theta}$ (nm)	hkl	I_{relative}							
			HAP	CTAB	P123	PEG	TWEEN	HDA	PAM	PVA
25.9	0.344	002	64	66	63	66	63	62	66	60
28.9	0.308	210	31	34	30	33	31	33	37	34
31.8	0.281	211	100	100	100	100	100	100	100	100
32.9	0.272	300	59	68	62	65	65	62	65	63
34.0	0.263	202	37	41	37	39	37	37	41	37
39.8	0.226	310	28	32	28	28	29	30	31	31
43.8	0.206	113	23	24	17	19	22	22	28	23
46.7	0.194	222	33	38	32	35	34	35	38	34
49.5	0.184	213	37	42	38	41	40	40	40	38
53.2	0.172	004	24	27	24	27	24	26	26	25
Mean crystallite particle size (nm)			25	25	16	24	23	25	20	21

Table 3. EDAX elemental analysis of HAP samples.

Sample	HAP	CTAB	P123	PEG	TWEEN	HDA	PAM	PVA	Ref [24]
Ca (wt%)	24.1	23.4	25.6	23.4	22.8	28.4	34.8	25.5	39.2
P (wt%)	14.5	14.6	13.9	13.9	13.2	15.9	16.6	14.5	18.2
Ca/P molar ratio	1.66	1.60	1.84	1.67	1.73	1.78	2.10	1.76	1.66

The BET surface areas and average particle size of samples prepared using different surfactants are shown in Table 4. Overall, the BET surface areas, 52-76 m² g⁻¹, are above the typical range reported for such materials, 20-60 m² g⁻¹. It is, of course, possible to prepare HAP with higher surface areas, but such reports frequently use relatively complicated procedures. For example, Jarudilokkul et al. prepared HAP with BET surface 227 m² g⁻¹, using a water in oil (W/O) emulsion liquid membrane system, which required (a) additional reagents to those used in our preparation, (b) ‘vigorous stirring’ and (c) 2 cycles of centrifugation to completely remove the organic membrane phase [22]. The BET surface area decreased to 58 m² g⁻¹ after thermal treatment similar to the conditions used in the preparation described here. Such thermal treatment is well known to reduce surface area, as reported previously by Kamieniak et al., which showed significant surface area reduction of HAP with increasing calcination temperature

for a similar preparation method to that reported here [30]. In all cases for the preparations in this paper, the addition of surfactant increases the surface areas, with the highest surface area recorded in the case of PEG. The straightforward addition of a surfactant during HAP synthesis is an improvement on the relatively onerous, conventional variation of experimental conditions such as: temperature, aging time, mixing order, pH, reactant addition rate, reactant concentration and calcination temperature. Uota and co-workers [27, 31-33] compared the use of a single surfactant versus a mixture of surfactants on the properties of HAP, the results of which showed that synthesis using mixed surfactants, nonaoxyethylene dodecyl ether (C₁₂EO₉) and polyoxyethylene sorbitan monostearate (TWEEN 60), produced the highest surface area HAP. In a similar study, Saha et al. proved that the surfactant plays an important role in the morphology and structure of HAP [33]. They synthesised HAP nanoparticles with four different surfactants using a reverse micelle method under different process conditions. The BET surface area of HAP was increased by the addition of NP5 (polyoxyethylene-nonylphenyl-ether) as surfactant, under optimised conditions (aqueous/organic ratio 1:5, pH 7, aging time 12 h and calcination at 450 °C). Surfactant addition affected the average particle size of synthesised samples, Table 4. The addition of CTAB, TWEEN and HDA surfactants led to increased particle size, relative to HAP, while the remaining surfactants caused a reduction. HAP particle size is known to affect its chemical and physical properties and, therefore, its effectiveness in any final application [34].

Table 4. BET surface areas and average particle size of HAP samples.

Sample	HAP	CTAB	P123	PEG	TWEEN	HDA	PAM	PVA
Surface area (m² g⁻¹)	52	65	68	76	69	67	58	68
Average particle size (µm)	2.22	2.82	1.80	1.85	2.92	3.20	2.13	2.01

N₂ adsorption-desorption, Figure 3, are typical type IV adsorption isotherms that confirm the presence of mesopores with type H1 hysteresis. These mesopores are formed by the voids between the particles, evidenced by the capillary condensation occurring at relative pressures 0.9 and above i.e. interparticular capillary condensation. Further proof of this is provided by the minimal adsorption at low pressures, as expected for densely formed crystalline HAP devoid of any significant amount of mesopores or micropores.

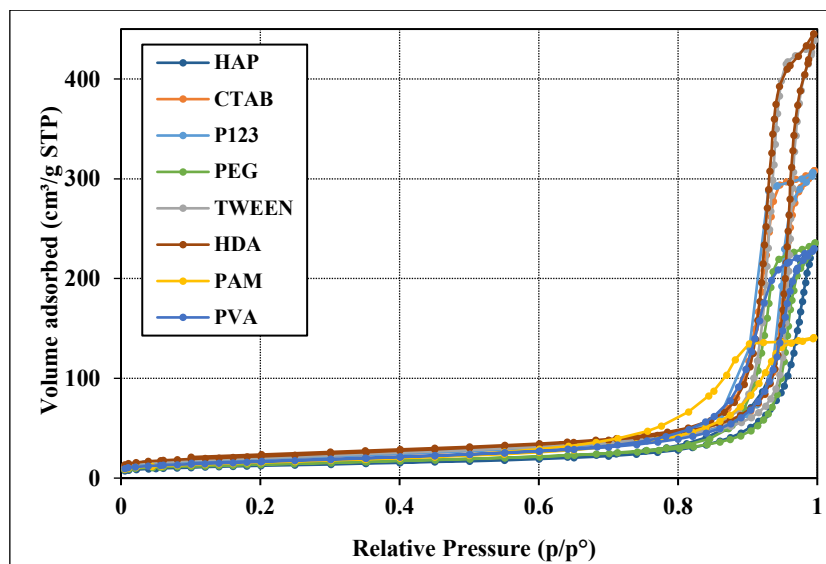


Figure 3. N₂ adsorption-desorption isotherms for HAP

SEM images of HAP samples synthesised with different templates are shown in Figure 4. Agglomerated particles are clearly visible on HAP prepared without surfactant, while surfactant-based samples have a more uniform structure.

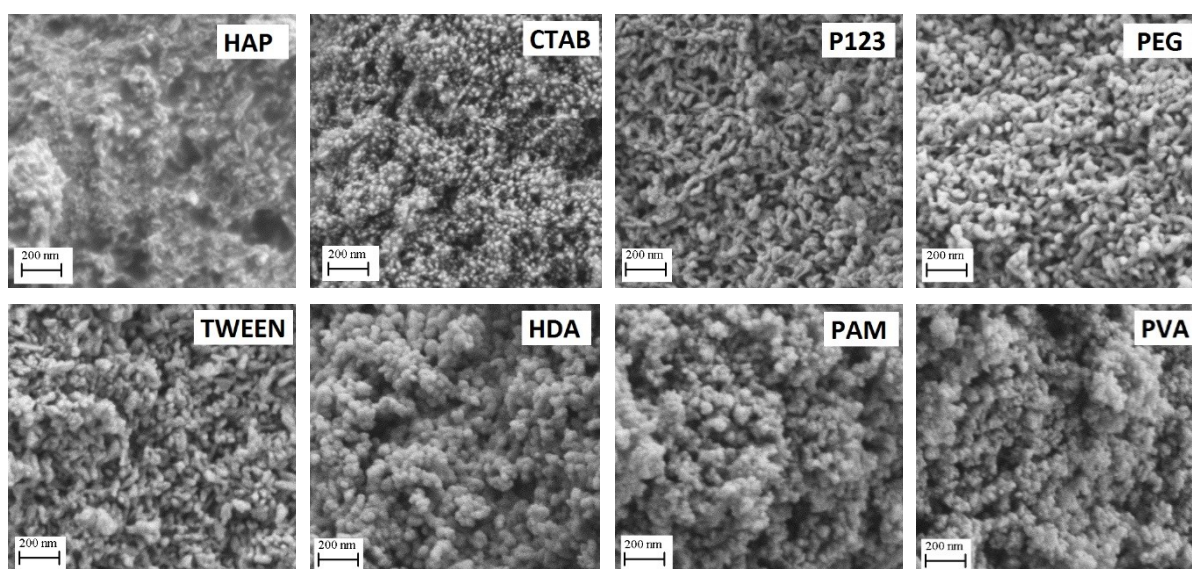


Figure 4. SEM images of hydroxyapatite samples synthesised with different surfactants

In order to understand the effect(s) of surfactant on the morphology and, therefore, other chemical and physical properties of HAP, the nucleation mechanism and growth of hydroxyapatite crystals is evaluated. It is known that when a surfactant is dissolved in water, cationic and non-ionic surfactant molecules form structures that minimise their surface tension. By increasing surfactant concentration to (and beyond) critical micelle concentration (CMC), ‘nano-reactors’ of surfactant assemblies are present inside the aqueous medium. Depending on the head group size of surfactant, ionic strength and

hydrophobic tail, the resulting assemblies, Figure 5, are known to have different shapes e.g. rod, spherical, worm-like or lamellar [35]. Phosphate precursors are then added to this surfactant solution, which adsorb onto the surfactant assembly surface due to electrostatic attractions between oppositely charged ions. Thereafter, the addition of calcium precursors results in calcium reaching the surface of surfactant assemblies containing phosphate to form layers of calcium phosphate, which is converted to HAP under the chosen synthesis conditions [35]. The surfactant in effect concentrates the phosphate and calcium precursors such that HAP formation occurs on this surface (although not exclusively). The morphology and surface properties of HAP prepared in the presence of surfactant are, therefore, influenced directly by the properties of the surfactant. Finally, the surfactant is removed by thermal decomposition in air (calcination).

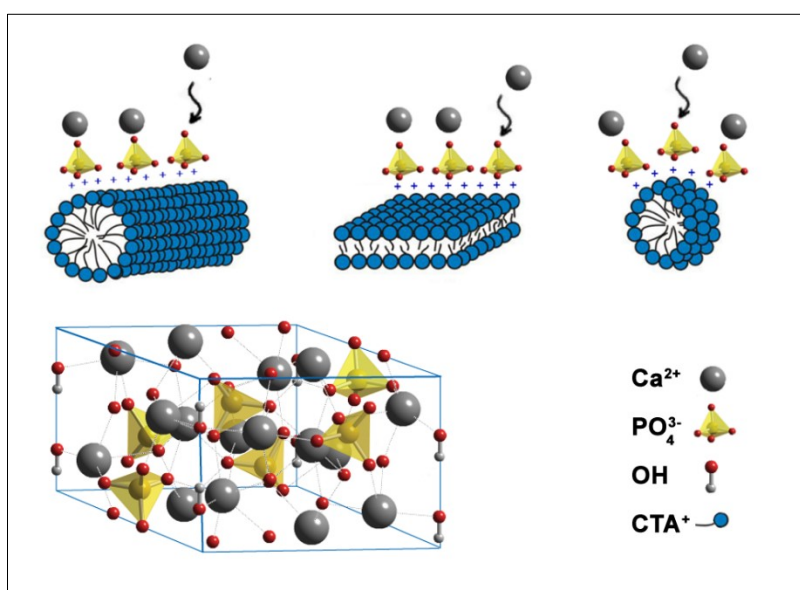


Figure 5. Nucleation and growth of hydroxyapatite crystals over cylindrical, bi-layers and spherical surfactant micelle.

3.2 CO oxidation

The catalytic activity of the HAP samples was tested in the oxidation of CO, Figure 6. Preparations using PEG, PVA and TWEEN caused a decrease in CO oxidation temperature; the temperature for 50% conversion, T_{50} , decreased from 340 °C for HAP prepared without surfactant to 320 °C for TWEEN and to 315 °C for both PEG and PVA. It is interesting to note that this trend towards lower temperature catalytic activity correlates with surface area increases from 52 m²g⁻¹ for HAP to 76, 68 and 69 m² g⁻¹ for PEG, PVA and TWEEN, respectively.

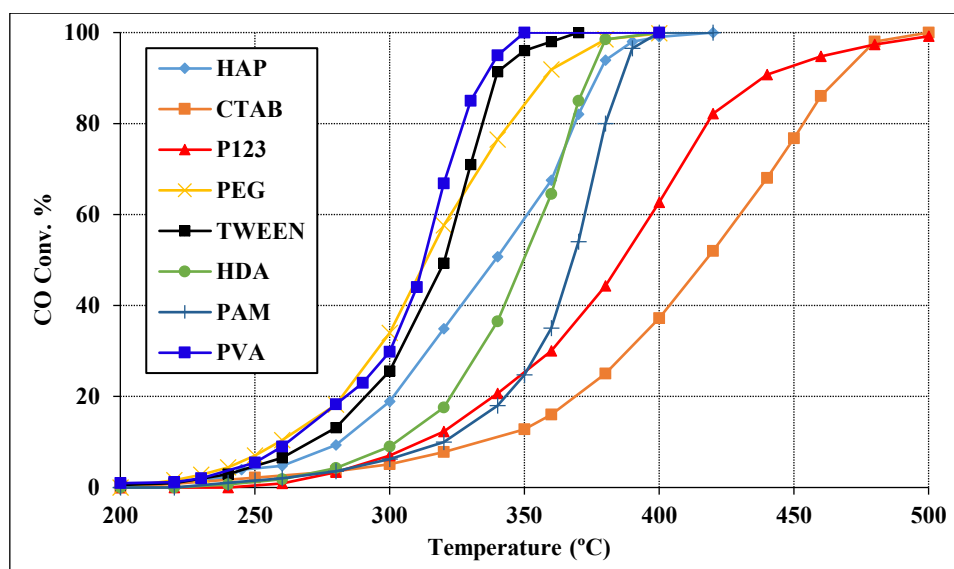


Figure 6. CO oxidation over different HAP samples.

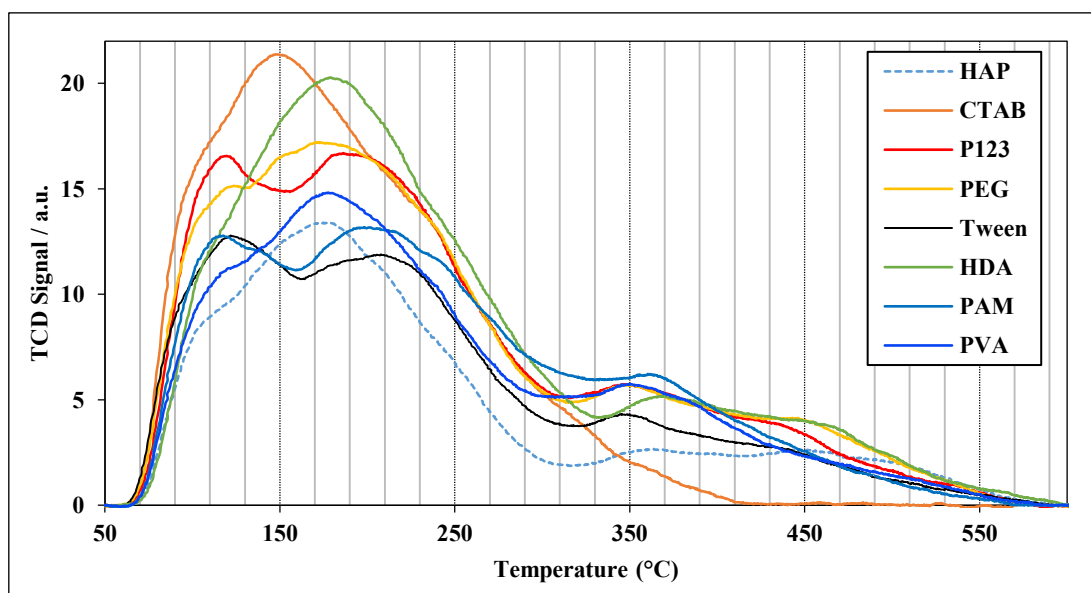


Figure 7. NH₃-TPD analysis of different HAP samples.

In the absence of metal nanoparticles, as is the case for the catalysts presented here, the acid sites on the HAP surface are considered to contribute to the CO oxidation adsorption and reaction. While a full understanding of the CO oxidation mechanism over acid sites on solid catalysts is still not entirely clear, the fact that CO has been used specifically as a probe molecule for acid site identification and quantification proves that CO adsorbs on acid sites [36]. Moreover, the CO oxidation reaction was shown to require the adsorption of CO on acid sites, and O₂ on basic sites, where the optimum catalytic activity occurred using equal densities of each surface site type [37, 38].

Both acidic and basic sites in HAP originate from POH–OH groups. FTIR analysis of HAP, using CO as a probe molecule, showed that the acidic PO–H groups on the HAP surface produce Brønsted acid sites. These acid sites are due to the phosphate rich terminations of the related powdered sample in which

these phosphate groups are protonated either once (HPO_4^{2-}) or twice (H_2PO_4^-) [39]. FTIR analysis of HAP using acetylene as probe molecule confirmed that the Brønsted basicity involved in catalytic reactivity was associated with bulk hydroxyl groups available on the channel surface. These basic OH^- groups are involved in two nondissociative adsorption modes of acetylene while there is no adsorption by PO_4^{3-} ; thus, the OH^- groups are considered to be the most likely basic active sites involved in catalytic reactions of Hap [40].

The acid sites were studied using NH_3 -TPD, Figure 7, to investigate the acid site strength and number, and explore the relation between acid site surface chemistry and CO oxidation activity. It has been shown that the accessibilities of Ca^{2+} (strong Lewis sites), and PO-H (weak/medium sites) are strongly dependent on the synthesis and drying parameters [41]. Therefore, the quantification of weak/medium and strong acid sites can provide useful insight into how surfactant addition can alter the acid sites distribution, such that the properties of HAP as heterogeneous catalyst can be tailored according to the requirement for Brønsted or Lewis acid sites.

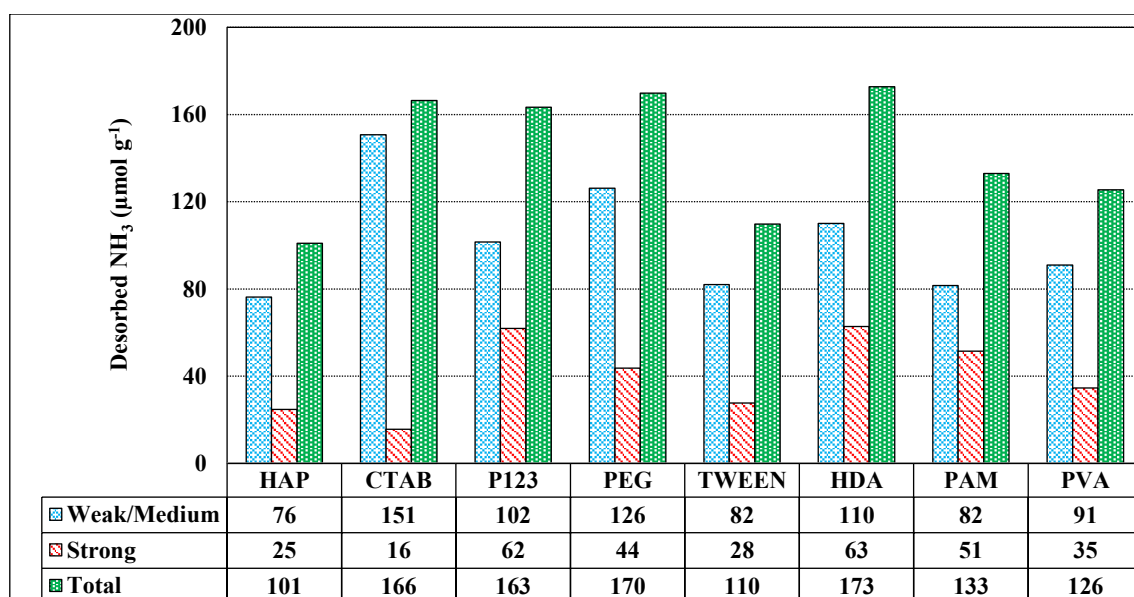


Figure 8. Quantitative analysis of acid sites over different HAP samples using NH_3 -TPD. ‘Weak/Medium’ and ‘Strong’ sites are assigned from desorption in the ranges 100-250 °C and >300 °C, respectively.

Figure 8 shows the acid site molar densities of the catalysts, where ‘weak/medium’ sites are in the range 100-250 °C, and ‘strong’ sites are >300 °C. Overall, the addition of surfactant has a significant effect on the total number and distribution of acid sites. All samples prepared with surfactant have higher quantities of total acid sites than HAP; these higher quantities correlate well with the higher surface areas recorded for the surfactant based syntheses. The NH_3 -TPD results are in good agreement with the Ca/P ratios from Table 3. For example, the lowest Ca/P ratio recorded for the CTAB sample, 1.60, contains the lowest quantity of strong acid sites, 16 $\mu\text{mol g}^{-1}$, and also has the lowest CO oxidation activity ($T_{50} = 415$ °C). However, a greater Ca/P ratio is not necessarily an indication of high catalytic

activity. Although the PAM sample has the highest Ca/P ratio (2.10), it is not the most active catalyst for CO conversion. This relatively low activity could be attributed (at least in part) to the low surface area of this sample ($58 \text{ m}^2 \text{ g}^{-1}$), which simply reduces the number of acid sites to catalyse the reaction. Comparing HAP again with the more active catalysts, there is a clear correlation between the decreasing T_{50} values and increasing quantities of each of the weak/medium, strong and total acid sites. For example, the total quantities of acid sites increased from $101 \text{ } \mu\text{mol g}^{-1}$ for HAP (T_{50} , $340 \text{ } ^\circ\text{C}$) to $110 \text{ } \mu\text{mol g}^{-1}$ for TWEEN ($320 \text{ } ^\circ\text{C}$), $126 \text{ } \mu\text{mol g}^{-1}$ for PVA ($315 \text{ } ^\circ\text{C}$) and $170 \text{ } \mu\text{mol g}^{-1}$ for PEG ($315 \text{ } ^\circ\text{C}$), Figure 9. A similar correlation is found between the light off temperatures measured at 10% conversion; T_{10} values decreased from $281 \text{ } ^\circ\text{C}$ for HAP to $271 \text{ } ^\circ\text{C}$ for TWEEN, $262 \text{ } ^\circ\text{C}$ for PVA and $259 \text{ } ^\circ\text{C}$ for PEG. These trends match with the results for increasing surface area, as increased surface area results in a greater number of acid sites on the surface. For the catalysts that were less active than HAP, our analysis of the numerical results showed that there does not appear to be any straightforward trend/correlation between the activities of the catalysts (as a group) and either the surface areas or acid site densities. It seems likely, therefore, that other factors may be responsible for the lower activity.

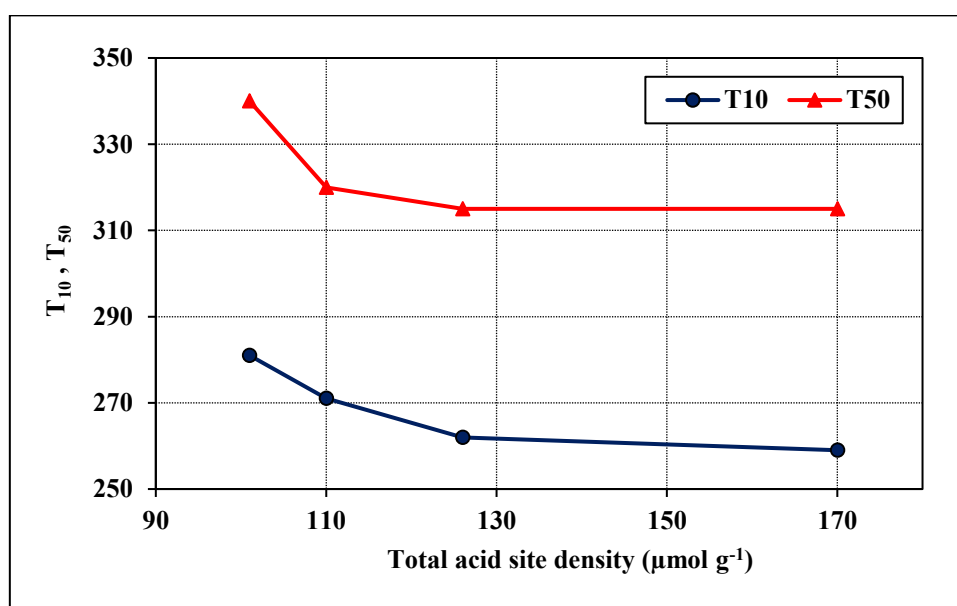


Figure 9. T_{10} and T_{50} values as a function of acid site density; samples are (from left to right) HAP, TWEEN, PVA and PEG.

4. Conclusions

This study shows the impact of using surfactants on the physical and chemical properties of hydroxyapatite for heterogeneous catalyst applications. Surfactants can change the morphology of the HAP by changing the nucleation and growth of hydroxyapatite crystals to cylindrical, bi-layers and spherical. Moreover, other properties of HAP such as surface area, Ca/P ratio, acid sites distribution and

strength are altered depending on the surfactant type, which consequently affects the catalyst activity of the HAP sample in oxidation reactions.

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